

# Rod eutectic growth in bulk undercooled melts

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## ABSTRACT

This article proposes an analytical model to understand the rod-growth of eutectic in the bulk undercooled melt. Based on the previous derivations of the lamellar eutectic growth models, relaxing the assumptions of small Peclet numbers, the model is derived by considering melt kinetic and thermal undercoolings. The intent of this model is to predict the transitions in eutectic pattern for conditions of the low and high growth velocity. In addition to investigation of the transition between lamellar and rod eutectic pattern, mathematical simplifications of solving Bessel function are presented as well, which is the most important priority to model calculation.

**Keywords:** Rod eutectic; growth; model; undercooling

## MSC CLASSIFICATION

80A22; 82C26

## 1 INTRODUCTION

Eutectic growth is characterized as two solid phases cooperatively grown from a liquid that is found in most of alloys [1]. The eutectic structures appeared as lamellar or rod-like morphologies, depend on actual solidification conditions[2]. To better understand the eutectic growth, Jackson and Hunt (JH-model) [3] first derived a model for lamellar and rod growth of eutectic in the diffusion-limited condition. Trivedi *et al.* (TMK-model) [4] extended JH-model to the process of rapid solidification.

Kurz and Trivedi [5] further considered the chemical distribution coefficient  $k$  as the function of growth velocity instead of its constant value being used in prior models. Later, a model considering the kinetic and thermal undercoolings was established by Li-Zhou *et al.* (LZ-model) [6,7] to depict the anomalous eutectics formed during solidification of undercooled melts. Moreover, Xu *et al.* [8,9] proposed a model attributed the suppression of eutectic decompositions to chemically partitionless solidification at a high growth velocity. Choudhury *et al.* [10] studied lamellar eutectic three-phase growth in ternary alloys.

As for rod growth of eutectic, the established models consider varied solidification conditions [11-13]. However, these models are basically obtained based on the JH model and using small Peclet numbers. Recently, Trivedi and Wang (TW) [14] relaxed the assumption of small Peclet numbers and obtained a model of rod growth even at high growth rates. However, their derivation is difficult to follow due to, (i) incomplete expression of the phase diagrams (i.e., cigar-shape and equal-distribution coefficients, (ii) lack of detailed Bessel function calculations [15], and (iii) neglect of thermal undercooling. Therefore, to develop a model based on TW and LZ model by addressing the shortcomings of the above-mentioned. Therefore, the present work is to attain this model for rod eutectic growth in bulk undercooled melts, especially at high growth rates.

## 2 MODEL EQUATIONS

Figure 1a presents a binary alloy system with elements A and B, having the specific eutectic concentration of  $C_E$  and equilibrium temperature of  $T_E$ . The  $\Delta C_\alpha$  and  $\Delta C_\beta$  represent the concentration differences between phases  $\alpha$ ,  $\beta$  and eutectic point, respectively. Figure 1b schematically illustrates the rod growth of eutectic, which is a kind of regular eutectic with couple growth [3]. The rod phase is denoted as the  $\alpha$ -phase with radius  $r_\alpha$ , while the matrix is the  $\beta$ -phase.

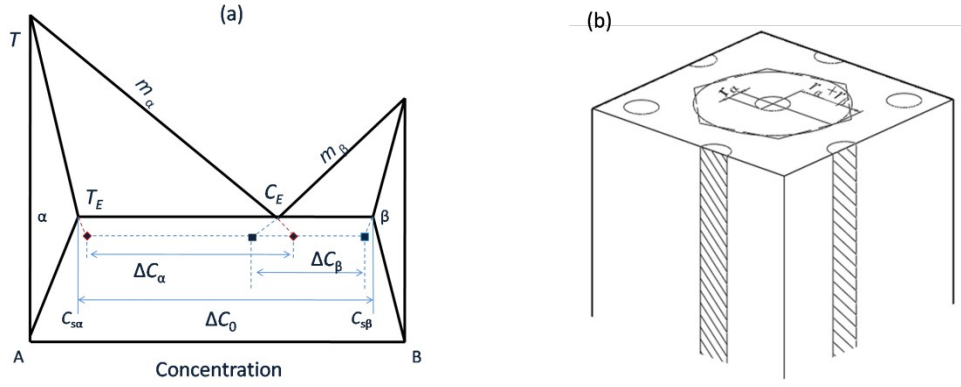


Fig. 1 (a) Eutectic phase diagram, and (b) schemata of a rod eutectic interface viewed normal to the interface.

Following the classical theory, the steady-state diffusion profile in the cylindrical coordinate system is governed by the equation [14]:

$$\left( \frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r} \right) + \frac{\partial^2 C}{\partial z^2} + \frac{V}{D} \frac{\partial C}{\partial z} = 0 \quad (1)$$

with the boundary conditions given by:

-periodicity:  $C(r+R)=C(r)$ , here  $R=(r_\alpha+r_\beta)$ ,

-symmetry:  $\partial C/\partial r=0$  for  $r=0$  and  $r=R$ ,

-far-field:  $C=C_\infty$  for  $z \rightarrow \infty$ ,

where  $C_\infty$  is the liquid composition far from the interface. The solution of the diffusion equation (1) is obtained as:

$$C = C_\infty + A_0 \exp\left(-\frac{Vz}{D}\right) + \sum_{n=1}^{\infty} A_n J_0\left(\frac{\gamma_n r}{R}\right) \exp(-\omega_n z) \quad (2a)$$

where

$$\omega_n = \frac{V}{2D} + \left[ \left( \frac{V}{2D} \right)^2 + \left( \frac{\gamma_n}{R} \right)^2 \right]^{1/2} \quad (2b)$$

Here  $A_0$  and  $A_n$  are the Fourier coefficients,  $J_0$  is the Bessel function of the zero order,  $Y_n$  is the  $n$ -th root of Bessel function of first order, i.e.  $J_1(Y_n)=0$ . According to the Supporting online materials,  $Y_n=3.144n+0.736$  ( $n=1,2,3,\dots$ ). The  $A_0$  and  $A_n$  are obtained from the condition of solute conservation at the solid/liquid interface [6] as,

-solute balance for  $\alpha$ -phase ( $0 \leq r < r_\alpha$ )

$$-D \left( \frac{\partial C}{\partial z} \right)_{z=0} = V(C_{l\alpha} - C_{s\alpha}) = VC(r, 0)(1 - k_\alpha) \quad (3a)$$

-solute balance for  $\beta$ -phase ( $r_\alpha \leq r < r_\alpha + r_\beta$ )

$$-D \left( \frac{\partial C}{\partial z} \right)_{z=0} = -V(C_{l\beta} - C_{s\beta}) = -V[1 - C(r, 0)](1 - k_\beta) \quad (3b)$$

where  $k_\alpha$  and  $k_\beta$  are the velocity dependent solute partitioning functions for  $\alpha$ -phase and  $\beta$ -phase, respectively, at the interface;  $C_{l\alpha}$  and  $C_{l\beta}$ ,  $C_{s\alpha}$  and  $C_{s\beta}$  are the concentrations of the  $\alpha$ -phase and  $\beta$ -phase in the liquid and solid, respectively.

To obtain the solution for  $A_0$  and  $A_n$ , we shall follow the treatments of TMK-model with the two special types of phase diagrams [4]. The first case is related to the cigar-shaped phase diagram and the second case is related to the equal distribution coefficients.

#### ***Case I: The cigar-shaped phase diagram [4]***

In this case, the solidus and liquidus are parallel below the eutectic temperature. One obtains  $C_{l\alpha} - C_{s\alpha} = \Delta C_\alpha = \text{const}$ , and  $C_{l\beta} - C_{s\beta} = \Delta C_\beta = \text{const}$  for any undercooling [8]. Then, Eq. (3) can be written as

$$\left( \frac{\partial C}{\partial z} \right)_{z=0} = \begin{cases} -\frac{V}{D} \Delta C_\alpha, & 0 \leq r < r_\alpha \\ \frac{V}{D} \Delta C_\beta, & r_\alpha \leq r < R \end{cases} \quad (4)$$

Combining Eqs. (2) and (4), the coefficient  $A_0$  and  $A_n$  can be thus given from Eq. (4) as

$$A_0 = f_\alpha \Delta C_\alpha - f_\beta \Delta C_\beta \quad (5a)$$

$$A_n = 4\sqrt{f_\alpha} \Delta C_0 \frac{J_1\left(\gamma_n \frac{r_\alpha}{R}\right)}{\gamma_n [J_0(\gamma_n)]^2} \left( \frac{1}{\sqrt{1 + p_n^2} + 1} \right) \quad (5b)$$

where  $p_n = 2\gamma_n/Pe$  and  $Pe$  is the Peclet number equals  $Pe = V\lambda/2D$ , and  $\lambda = 2R$ .

**Case II: The diagram with equal distribution coefficients for the two phases [4]**

For this case,  $k$  is an arbitrary constant, but  $k_\alpha = k_\beta = k_e$ , and  $C(r,0) = C_\infty/k$ . Then Eq. (3) can be written as

$$\left( \frac{\partial C}{\partial z} \right)_{z=0} = \begin{cases} -\frac{V}{D} \frac{C_\infty}{k} (1-k), & 0 \leq r < r_\alpha \\ \frac{V}{D} \frac{1-C_\infty}{k} (1-k), & r_\alpha \leq r < R \end{cases} \quad (6)$$

Using Eqs. (2) and (6), one arrives at

$$A_0 = \frac{(1-k)}{k} \frac{C_\infty r_\alpha^2 - (1-C_\infty)[(r_\alpha + r_\beta)^2 - r_\alpha^2]}{(r_\alpha + r_\beta)^2}$$

(7a)

$$A_n = 4\sqrt{f_\alpha} (1-k) \frac{J_1\left(\gamma_n \frac{r_\alpha}{R}\right)}{\gamma_n [J_0(\gamma_n)]^2} \left[ \frac{1}{\sqrt{1 + p_n^2} - 1 + 2k} \right] \quad (7b)$$

where  $C_\infty$  is the liquid compositions far away from the S/L interface.

For the undercooling calculation, the interfacial average composition in liquid is obtained from the LZ treatment [6]. Using Eq. (2a) and the Fourier coefficient for Cases I and II, the average compositions in the liquid at the interface ahead of the  $\alpha$  and the  $\beta$  phases are obtained as

$$\bar{C}_\alpha = C_\infty + A_0 + \frac{4V(r_\alpha + r_\beta)}{D} \Delta C_0 M \quad (8a)$$

$$\bar{C}_\beta = C_\infty + A_0 - \frac{4r_\alpha^2(r_\alpha + r_\beta)}{(r_\alpha + r_\beta)^2 - r_\alpha^2} \frac{V \Delta C_0 M}{D} \quad (8b)$$

where the function  $M$  for rod eutectic has two cases expression for the phase diagrams. These are:

**Case I: The cigar-shaped phase diagram**

$$M = \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2} \left[ \frac{P_n}{\sqrt{1 + P_n^2} + 1} \right] \quad (9a)$$

$$M + R \frac{\partial M}{\partial R} = \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2} \left[ \frac{P_n}{\sqrt{1 + P_n^2} + 1} \right]^2 \frac{P_n}{\sqrt{1 + P_n^2}} \quad (9b)$$

**Case II: The diagram with equal distribution coefficients for the two phases**

$$M = \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2} \left[ \frac{P_n}{\sqrt{1 + P_n^2} - 1 + 2k} \right] \quad (10a)$$

$$M + R \frac{\partial M}{\partial R} = \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2} \left[ \frac{P_n}{\sqrt{1 + P_n^2} - 1 + 2k} \right]^2 \frac{P_n}{\sqrt{1 + P_n^2}} \quad (10b)$$

Then the interfacial undercooling for each phase can be obtained as:

$$\Delta T_\alpha = m_\alpha^v [\bar{C}_\alpha - C(r, 0)] + \frac{2a_\alpha^R}{r_\alpha} + \frac{V}{\mu_\alpha} \quad (11)$$

$$\Delta T_\beta = m_\beta^v [C(r, 0) - \bar{C}_\beta] + \frac{2a_\beta^R r_\alpha}{(r_\alpha + r_\beta)^2 - r_\alpha^2} + \frac{V}{\mu_\beta} \quad (12)$$

Where  $\mu_\alpha$  and  $\mu_\beta$  are the kinetic coefficient;  $a_\alpha^R = \Gamma_\alpha^R \sin \theta_\alpha^R$  and  $a_\beta^R = \Gamma_\beta^R \sin \theta_\beta^R$ , are the Gibbs-

Thompson relationship for  $\alpha$  and  $\beta$  phases;  $m_\alpha^v$  and  $m_\beta^v$  are the liquidus slope dependent on growth velocity, respectively. Given  $\Delta T_\alpha = \Delta T_\beta = \Delta T_I$  for eutectic growth, eliminating  $C(r,0)$  in Eqs. (11) and (12), the interface undercooling can be obtained as

$$\Delta T_I = m^v \left[ \left( Q_0^R R + \frac{1}{\mu} \right) V + \frac{a^R}{R} \right] \quad (13a)$$

$$a^R = 2\sqrt{f_\alpha} \left( \frac{a_\alpha^R}{f_\alpha m_\alpha^v} + \frac{a_\beta^R}{f_\beta m_\beta^v} \right) \quad (13b)$$

$$m^v = \frac{m_\alpha^v m_\beta^v}{m_\alpha^v + m_\beta^v} \quad (13c)$$

$$\mu = \frac{m_\alpha^v m_\beta^v \mu_\alpha \mu_\beta}{m_\alpha^v \mu_\alpha + m_\beta^v \mu_\beta} \quad (13d)$$

For Case I, since  $\Delta C_\alpha + \Delta C_\beta = \Delta C_0$ , thus it arrives at:

$$Q_0^R = \frac{4\Delta C_0}{f_\beta D} M \quad (13e)$$

For Case II, since  $\Delta C_0 = 1 - k$ :

$$Q_0^R = \frac{4(1-k)}{f_\beta D} M \quad (13f)$$

Similar to the treatment for lamellar eutectic in LZ model [6], considering the thermal undercooling, we have:

$$\Delta T = \Delta T_c + \Delta T_r + \Delta T_k + \Delta T_i = m^v \left[ \left( Q_0^R R + \frac{1}{\mu} \right) V + \frac{a^R}{R} \right] + \frac{\Delta H}{C_p} Iv(P_i) \quad (14)$$

where  $\Delta H = f_\alpha \Delta H_\alpha + f_\beta \Delta H_\beta$ , is the weighted heat of fusion of two eutectic phases and  $C_p$  is the specific

heat of the liquid,  $Iv$  is the Ivantsov function,  $Iv(u) = u \exp(u) E_1(u)$ , in which  $E_1(u) = \int_u^\infty \exp(-v) / v dv$  is the first exponential integral function.  $P_t$  denotes the thermal Peclet number [8].

To analyze the behaviour of rod spacing  $R$ , from the minimum undercooling principle and Eq. (14), we obtained relationship for the rod spacing as a function of velocity [6]:

$$VR^2 = a^R / Q^R \quad (15)$$

For Case I:

$$Q^R = \frac{4\Delta C_0}{f_\beta D} \left( M + R \frac{\partial M}{\partial R} \right) \quad (16a)$$

For Case II:

$$Q^R = \frac{4(1-k)}{f_\beta D} \left( M + R \frac{\partial M}{\partial R} \right) \quad (16b)$$

From Eqs. (14)-(16), the relationship of undercooling and interlamellar  $\Delta T$ - $R$  can be obtained as

$$\Delta T = m^v \frac{a^R}{R} \left( 1 + \frac{M}{M + R(\partial M / \partial R)} + \frac{1}{\mu Q^R R} \right) + \frac{\Delta H}{C_p} Iv(P_t) \quad (17)$$

As a result of solutions (14)-(17) together with Eqs. (9) and (10), we can determine the growth velocity  $V$  and rod spacing  $R$  as functions of the melt undercooling  $\Delta T$ . Neglecting the effect of thermal undercooling, the system of equations (14)-(17) transforms to the expression  $\Delta T$ - $V$ - $\lambda$  previously obtained in TW-model[14], note that  $\lambda=2R$  for rod eutectic.

For the present model, the slope of the liquidus line  $m^v$  is dependent on the growth velocity. It can be given as [16]:



$$m^v = m \left\{ 1 + \frac{k_e - k[1 - \ln(k/k_e)]}{1 - k_e} \right\}, \quad (18)$$

where  $k$  is the solute segregation coefficient dependent on the growth velocity:

$$k = \frac{k_e + V/V_{DI}}{1 + V/V_{DI}} \quad (19)$$

where  $V_{DI}$  is the diffusion speed at the interface[16].

Using the same parameters of  $f_\alpha/C_{s\alpha}/C_{s\beta}/C_E/C_\infty/m_\alpha/m_\beta/T_E/\mu/D_0/E/V_{DI}=0.25/0.02/0.98/0.74/0.74/450/450/1400/0.01/8.0 \times 10^{-8}/5 \times 10^4/0.5$ , the growth velocity as the function of undercooling are calculated by JH model[3] and the present model Eq.(17), as shown in Fig. 2a. The results of Eq.(7) is coincident with the JH-model as the undercooling ( $\Delta T$ ) below  $\sim 150$  K, then showing increasing deviations as  $\Delta T$  rising until 400 K. This is a consequence of the relaxations of Peclet numbers. The eutectic rod spacing as the function of growth velocity is shown in Fig. 2b, it can found that the rod spacing result from the present model is small than that from JH model.

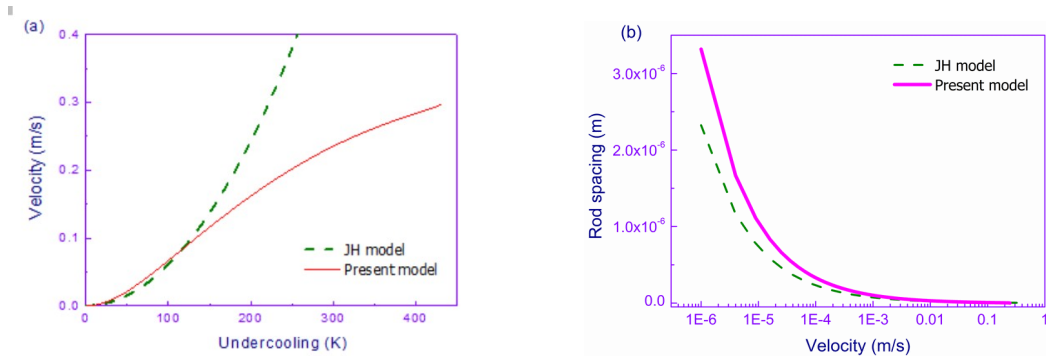


Fig.2 Model calculation of JH model and the present model for different growth velocity: (a)  $V-\Delta T$ ;  
(b)  $R-V$

Moreover, the present model is approximately identical to the lamellar growth of eutectic as incorporating kinetic and thermal undercoolings upon solidification into the model. To study the phase selection of rod and lamellar eutectic, one needs to figure out the relationship between the growth velocity and undercooling for the two models. For LZ model, the lamellar eutectic growth relation can be given as [6]:

$$\Delta T^L = m \left( \frac{\Delta C_0 P}{f_\alpha f_\beta D} \lambda + \frac{1}{\mu} \right) V + m \frac{a^L}{\lambda} + \frac{\Delta H}{C_p} \ln(P_i) = f^L(V, f_\alpha) \quad (20a)$$

For the present rod eutectic model, the similar form can be written as:

$$\Delta T^R = m \left( \frac{4\Delta C_0 M}{f_\beta D} R + \frac{1}{\mu} \right) V + m \frac{a^R}{R} + \frac{\Delta H}{C_p} \ln(P_i) = f^R(V, f_\alpha) \quad (20b)$$

As is known, if several structures compete at a given growth rate, the structure that requires the lowest  $\Delta T$  will grow preferentially. Thereafter, if we calculate  $\Delta T$  via Eq. (20) at a fixed growth velocity and variation of  $f_\alpha$ , it is possible to predict structural preference in normal eutectic growth. The lowest  $\Delta T$  corresponds to the winning growth mode. Thus, we use a group calculation to show the transition in between the rod and lamellar eutectic.

Using Eq.(20) with Case I phase diagram expressions and parameters of  $C_{s\alpha}/C_{s\beta}/m_\alpha/m_\beta/k_\alpha/k_\beta/V_{DL}/T_E/\mu/D_0/E=0.02/0.98/450/450/0.0226/0.1724/0.5/1400/0.01/8.0 \times 10^{-8}/5 \times 10^4$ , the relationship of  $\Delta T$ - $V$ - $\lambda(R)$  is given as shown in Fig.3a. It can be found that the surface diagram of  $\Delta T^R=f^R(V, f_\alpha)$  and  $\Delta T^L=f^L(V, f_\alpha)$  have a common line of intersection at about  $f_\alpha=0.2\sim 0.35$ , which is corresponding to critical fraction values  $f_\alpha^*$  for the rod-lamellar eutectic transition at different  $V$ . At a constant  $V$ , if  $f_\alpha < f_\alpha^*$ , the undercooling of rod eutectic is lower, so the alloy solidifies with rod eutectic structure; instead, if  $f_\alpha > f_\alpha^*$ , the alloy solidifies with normal lamellar eutectic structure.

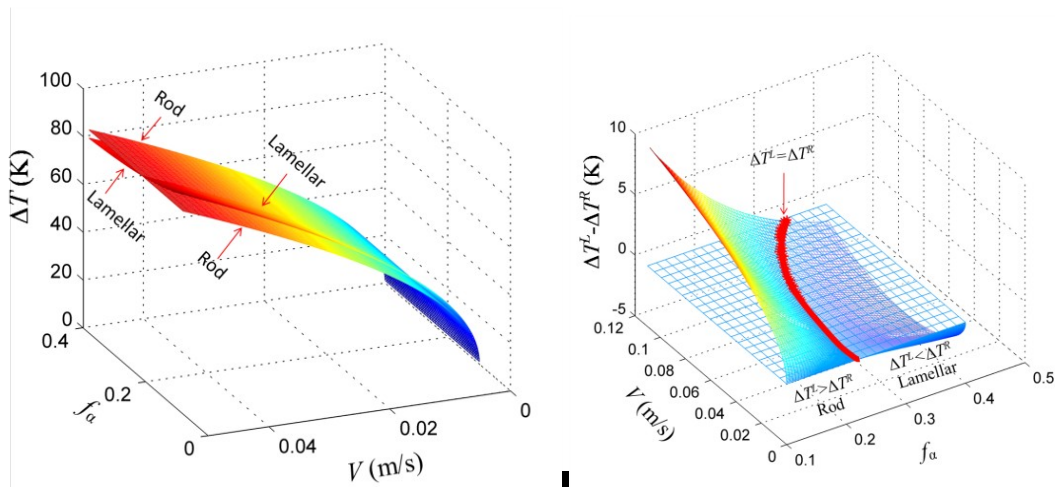


Fig. 3 The calculation result of rod eutectic model and lamellar eutectic model: (a) the surface diagram of  $\Delta T^R=f^R(V,f_a)$  and  $\Delta T^L=f^L(V,f_a)$ ; (b) the surface diagram of  $\Delta T^R-\Delta T^L$  change with  $V$  and  $f_a$ .

From the above description, the one with the same growth velocity and low  $\Delta T$  wins. Compare Eq. (20a) (LZ model) with Eq. (20b) (present model), the kinetic and thermal undercoolings expressions are totally same, subtracting the two equations thereby leading to,

$$\Delta T^L - \Delta T^R = m \left( \frac{\Delta C_0 P}{f_\alpha f_\beta D} \lambda - \frac{4 \Delta C_0 M}{f_\beta D} R \right) V + m \left( \frac{a^L}{\lambda} - \frac{a^R}{R} \right) = f(V, f_\alpha) \quad (21)$$

Thus, the critical fraction  $f_a^*$  for rod-lamellar transition can also be found by plotting

$\Delta T^L - \Delta T^R = f(V, f_\alpha)$ , as shown in Fig. 3b. The red line is the position when  $f(V, f_\alpha) = 0$ , which

represents the critical fraction value  $f_a^*$  at varying  $V$ . When  $f_a$  is larger than  $f_a^*$ , there is  $\Delta T^L > \Delta T^R$ , so the rod eutectic win in the final structure; on the opposite, the lamellar structure will form. It's worth noting that the critical fraction  $f_a^*$  increases from 0.2 to 0.35 with increase of growth velocity, which is consistent with Lei's predictions [17]. It indicates that the rod-lamellar transition is dependent on both  $\alpha$ -phase fraction and the eutectic growth velocity.

Equations (9), (10), (13), (16) include the function M, which is determined by Bessel function  $J_1(Y_n)$ .

The series expansions for Bessel function are expressed as following [18],

$$J_0(x) = \sum_{m=0}^{\infty} \frac{(-1)^m}{(m!)^2} \left( \frac{x}{2} \right)^{2m} \quad (22a)$$

$$J_1(x) = \sum_{m=0}^{\infty} \frac{(-1)^m}{m!(m+1)!} \left( \frac{x}{2} \right)^{2m+1} \quad (22b)$$

Accordingly, it is difficult to solve Eq. (22) as it's not easy to obtain the root of equation  $J_1(x)=0$ , i.e. the values of  $Y_n$ . As the ' $Y_n$  approximately equal to  $n\pi$ ' by Jackson [3], which was also widely used by

other models [12,13]. Using computer program, we obtain the result  $\gamma_n$  as calculating the root of  $J_1(x)=0$  by Eq. (22b) for  $n=1,2,3... 20$ , as:

$\gamma_n=[3.83170597020751, \quad 7.01558666981562, \quad 10.1734681350627, \quad 13.3236919363142,$   
 $16.4706300508776, 19.6158585104682, 22.7600843805928, 25.9036720876184, 29.0468285349169,$   
 $32.1896799109744, \quad 35.3323075500839, \quad 38.4747662347716, \quad 41.6170942128145,$   
 $44.7593189976528, 47.9014608871855, 51.0435351835715, 54.1855536410613, 57.3275254379010,$   
 $60.4694578453475, 63.6113566984812].$

The calculated results are shown in Fig. 4a. It can be seen that the calculated  $\gamma_n$  are larger than those given by Jackson et. al [3] model, but they are approximately equal to those shown in the Handbook [15]. By fitting with calculated values, we obtained  $\gamma_n=3.144n+0.736(n=1,2,3...)$ . This easily facilitates the calculations for equations related to the Bessel function, such as the  $M$  value in JH model:

$$M_{JH} = \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2} = \frac{[J_1[(3.144n + 0.736)\sqrt{f_\alpha}]^2}{(3.144n + 0.736)^3 [J_0(3.144n + 0.736)]^2} \quad (23)$$

In the present study, Eqs. (2), (5), (7), (9), (10) can be easily calculated by Eq. (23) treatment.

Figure 4b presents the  $M$  of JH model ( $\sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2}$ ) as function of  $\alpha$  phase fraction. It can be found that  $M$  value from  $\gamma_n=3.144n+0.736$  ( $n=1,2,3...$ ) is nearly the same to that from Table I in Ref. [3]. However, if  $\gamma_n \sim n\pi$  is used, the results are deviated from the true value by more than twice (Fig.4b). This further suggests using  $\gamma_n=3.144n+0.736$  for Bessel function in the rod eutectic growth model (that is more accurately than  $\gamma_n \sim n\pi$ ).

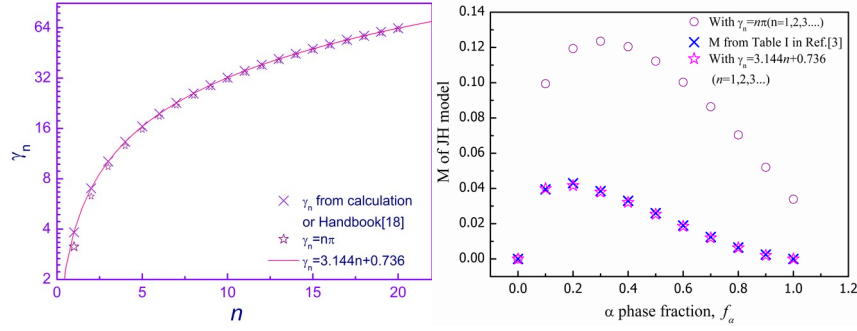


Fig. 4(a) The  $\gamma_n$  values from different methods; (b) M of JH model (
$$= \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_\alpha})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2}$$
) calculated

with different expression of  $\gamma_n$  values

### 3 CONCLUSIONS

By relaxing the small Péclet number assumptions, the rod eutectic growth model is developed for the growth velocity and inter rod spacing by considering the kinetic and thermal undercooling in bulk undercooled melts. A simple expression for the equation related to Bessel function is given and the root  $\gamma_n = 3.144n + 0.736$  ( $n = 1, 2, 3, \dots$ ) is found for Bessel function  $J_1(x) = 0$ , which can also simplify the calculation of the other rod eutectic models. The rod-lamellar eutectic transition has been calculated by combining LZ model and the present model. It shows that the critical phase fraction (about  $f_\alpha^* = 0.2$ -0.35 here) increases with growth velocity. The developed model can be further extended to the eutectic solidification under local non-equilibrium conditions in the diffusion field as it has been formulated and summarized in Ref. [19].

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## Figure captions

Fig. 1 (a) Eutectic phase diagram, and (b) schemata of a rod eutectic interface viewed normal to the interface.

Fig.2 Model calculation of JH model and the present model for different growth velocity: (a)  $V$ - $\Delta T$ ; (b)  $R$ - $V$

Fig. 3 The calculation result of rod eutectic model and lamellar eutectic model: (a) the surface diagram of  $\Delta T^R = f^R(V, f_a)$  and  $\Delta T^L = f^L(V, f_a)$ ; (b) the surface diagram of  $\Delta T^R - \Delta T^L$  change with  $V$  and  $f_a$ .

Fig. 4 (a) The  $\gamma_n$  values from different methods; (b) M of JH model (
$$= \sum_{n=1}^{\infty} \frac{[J_1(\gamma_n \sqrt{f_a})]^2}{\gamma_n^3 [J_0(\gamma_n)]^2}$$
) calculated

with different expression of  $\gamma_n$  values



## **Authorship**

Authors contributed equally to the content of the manuscript.